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CFD-DEM MODELING OF THE GRAVEL PACKING PROCESS DURING PETROLEUM HORIZONTAL WELL COMPLETIONS

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Abstract: The increasing exploration challenges, faced by the oil industry, require the development of new technologies to achieve higher efficiency in the extraction of oil and gas, contemplating the lowest possible cost. Numerical simulation of processes exist to help solving several problems faced by industries, and is capable of accomplishing different virtual try-outs, which can provide answers to understand and optimize the process in discussion. With the expressive development of computers capabilities, the simulation field that most called attention in the last years has been the Computational Fluid Dynamics (CFD), which can computationally reproduce complex fluid flows involving turbulence, reactions, multiphase system, etc. One of the gaps still faced by the modern CFD codes is the incapacity of simulating in details the multiphase systems involving granular solids, which are common in many industry processes, especially in the oil and gas industry. The present paper holds as its objective to develop a new methodology to numerically reproduce granular flows, addressing a different tool to help during the calculation: the so called Discrete Element Method (DEM), used to perform particles simulation. As an adopted methodology, a coupling between CFD (Fluid Flow Calculation) and DEM (Particle Tracks Calculation) is performed. To assess and validate the approach proposed, the Gravel Packing process of horizontal wells was used as a test for the simulations of the present work, which is widely used by Petrobras for completion deepwater and ultra-deep water wells which requires a better comprehension to search more efficient and economical considerations. The obtained results in the present work turned out to be very much promising, which means that it is possible to work numerically with the complex problem of high solids concentration. The main results of this study show a validation of the alpha wave height obtained in numerical simulation within simulators data of Petrobras. The results proved the applicability of the approach and that the CFD-DEM coupling may, in the future, be used to aid in the design operation of gravel packing in horizontal wells.

1 INTRODUCTION

Gravel packing is today the most frequently applied sand control technique in Campos Basin, offshore Brazil. Because of the critical conditions, such as the deep and ultra deep waters and low fracture gradients, great precision is required to assure gravel-packing success. The sand production during exploration turns sometimes unviable the oil extraction. A common problem occurs when the separation equipment is not enough to permit the continuum operation.

The gravel packing process is illustrated in the Figure 1.

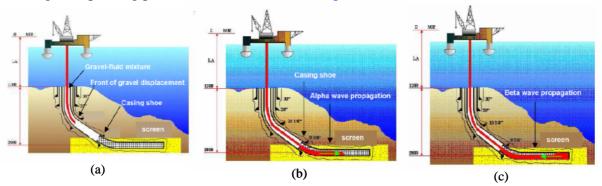


Figure 1 – Stages during gravel packing process. (a) Proppant injection; (b) Alpha wave displacement; (c) Beta wave displacement

The operation consists of filling the annulus formed between the open reservoir and the screen with particulate material (known as proppant). The particulate acts as a filtering region, permitting only the petroleum flows throughout the production column. The Figure 1 (a) shows the sand-liquid mixture being injected in the platform. In the Figure 1 (b), the proppant settles in the bottom of the annulus, due the gravity effects (alpha wave propagation). Figure 1 (c) shows the solids filling the top of the annulus (beta wave propagation). The gravel packing column has several components, which allow the solid-liquid mixture flow in the annulus correctly. Figure 2 shows de main components of the process.

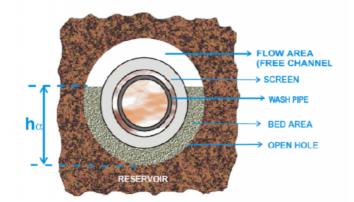


Figure 2 – Gravel packing components

To help in the design of the gravel packing process, several models are available in the industry; nevertheless, they are essentially empirical, resulting in imprecise predictions for extrapolated conditions. There are also some mechanistic models, but that models are not able to describe operational details, such as alpha wave height and conditions where the premature screen out occurs.

Looking for better comprehension of the process, and to get parameter do adjust Petrobras'

Mechanistic Model, Petrobras and ESSS have been developed a CFD-DEM model to reproduce numerically the multiphase flow in the gravel packing operation. The approach consists in the coupling between computational fluid dynamics and discrete element model. This new methodology permit evaluate de the details of the solid flow, such as particle-particle interaction and particle-fluid interaction. The goal of the study is forecast the solid bed height under different operational conditions. These data can be compared with experimental data provided by Petrobras engineers, so that the approach can be validated. The steps of the methodology will be listed below.

2 METHODOLOGY

In the present study, the objective is reproduce the gravel packing process, so that it will be possible to get data that can help in the design of the practical operation.

Nevertheless, a lot of challenges are present in this multiphase flow modeling. Some examples:

- Granular solids flowing under different regimes. The presence of high solid volume fraction and stagnated flow is very problematic for numerical simulations;
- The size of the problem. The gravel packing process is operated in large well sections, which is not feasible in numerical simulations using CFD;
- The total number of particles is very high, turning computational simulation very expensive.

In this way, a simplified case has been studied, looking for less computational effort, but without lose in the quality of final results.

2.1 Geometry

The gravel packing process scheme is illustrated in Figure 3.

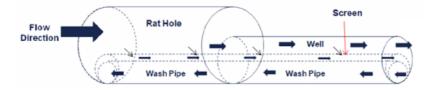


Figure 3 - Gravel packing scheme

In this study case, the analysis will take place at the contraction region (rat hole/open hole transition). The 3D simulation is not feasible, due the high number of particles. A 2D domain is proposed, and showed in Figure 4.

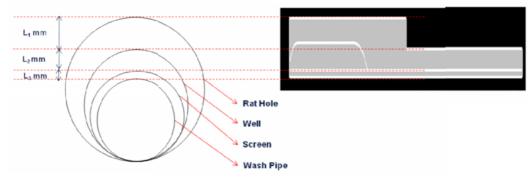


Figure 4 – Simplified geometry in CFD simulations

2.2 Computational mesh

The computational mesh results of the geometry discretization, which goal is divide the domain in small enough elements, where the conservation equations will be applied to obtain the flow profiles.

In order to get an optimal discretization, it has been generated a hexa mesh into the geometry. In the structured mesh, the discrete elements are aligned with the flow, what help in the problem convergence. Figure 5 shows some images of the computational mesh performed for the gravel packing simulation. The final mesh has a size of 24.000 elements.

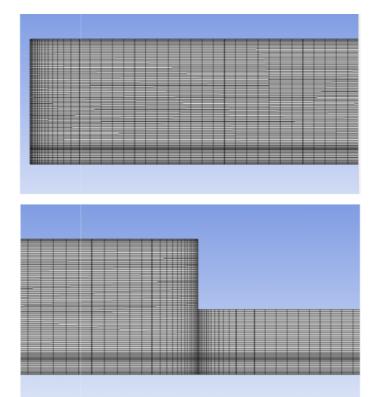


Figure 5 – Computational mesh

2.3 Physical set up

The problem set up has been proposed according to the operational data provided by Petrobras. In CFD-DEM approach, the results are obtained through of two software calculations: Fluent, from ANSYS Inc (CFD Side); and EDEM, from DEM Solutions (DEM Side).

The fluid flow is solved through the momentum balance (Navier-Stokes equations), showed in the Equation (1).

$$\frac{\partial \varepsilon_f \rho U}{\partial t} + \nabla . \left(\varepsilon_f \rho U U \right) = -\nabla P + \nabla . \left(\mu_{eff} \left(\varepsilon_f \nabla . U \right) \right) + \rho \varepsilon_f g - S \tag{1}$$

The equation above is the traditional momentum equation, where de $_f$ denotes the fluid volume fraction. *S* is the source term (the particle influence into the fluid flow will take place in this term).

On each particle, it will be applied a force balance (all the forces acting in the particle: contact, non-contact, drag, etc.). Therefore, DEM will basically solve two equations, which

perform the particle track inside the domain: Equation (2) for translational movement and Equation (3) for rotational movement.

$$F = m \frac{\partial}{\partial t} \left(\frac{\partial r}{\partial t} \right) \tag{2}$$

$$I\frac{\partial \boldsymbol{\varpi}}{\partial t} = \sum \boldsymbol{M} \tag{3}$$

During the calculation, a coupling module promotes the interaction between the phases. This coupling is made through the additional sources terms in the fluid equations, exchanging momentum with the particles via drag forces.

The coupling module also returns the solid and fluid volume fraction, through the average number of particles inside each fluid computational cell.

The assumptions made in these CFD-DEM simulations are described below.

CFD Side

- Symmetry condition
- Constant fluid properties (specific mass, viscosity)
- Turbulent flow regime (k- model)
- Boundary Conditions
 - o Inlet: Prescribed velocity
 - o Outlet: Prescribed pressure
 - Walls: No slip condition
- Ansys Fluent software

DEM Side

- Periodic condition
- Constant particle shape (no particle deformation)
- Spherical particle, with just one particle diameter
- No slip among particle and geometry
- Particle generation rate constant
- DEM Solutions EDEM software

The application of the boundary condition is showed in Figure 6.

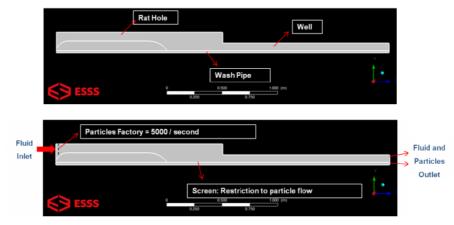


Figure 6 - Simulation boundary conditions

Different cases have been simulated, evaluating the operational conditions influence in the rat hole solid bed height. The operational conditions simulated are listed below:

<u>Case 1</u> Particle Diameter: 630 μm Particle Density: 2,71 Fluid Flow: 6 BPM

Case 2 Particle Diameter: 630 μm Particle Density: 2,71 Fluid Flow: 7 BPM Case 3

Particle Diameter: 630 μm Particle Density: 2,71 Fluid Flow: 8 BPM

<u>Case 4</u> Particle Diameter: 950 µm

Particle Density: 1,89 Fluid Flow: 6 BPM

2.4 Results

The CFD-DEM results supply detailed information about the fluid and solid flow into the domain. Profiles of velocity, volume fraction, pressure, turbulence are easily obtained with numerical simulations. The CFD analysis of this study is concentrated in the velocities profiles and solid volume fraction profile, due the interest in evaluate different flow regimes and the solids bed height.

Figure 7 shows Case 1 flow profile snapshots. It is possible identify that the bed grows until the fluid flow reaches a critical velocity. In that point, the fluid velocity is sufficiently high to guarantee the horizontal solid transport. The same behavior is observed in the others simulated cases.

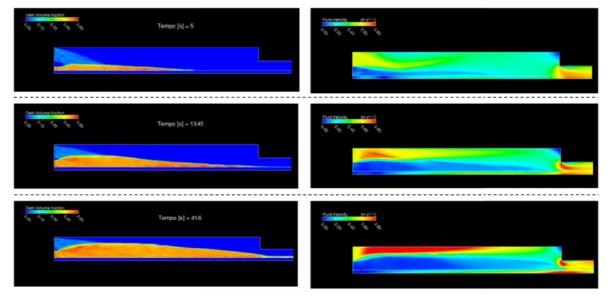


Figure 7 – Simulated flow profile

This stable situation occurs due the drop pressure equilibrium between the fluid flowing above the solid bed and the fluid flowing in the wash pipe. The simulation result shows that when solids particles start settling in the screen, the fluid velocity in the wash pipe starts to become higher.

In order to evaluate the bed height in the simulations, five analysis positions have been marked in the rat hole, according with Figure 8. These five position time-evolution of the bed height is showed in Figure 9. The total stability have not been reached in all rat hole channel,

but at Point 1 and Point 2, the bed height is stabilized since 25 seconds. Therefore, the bed height has been evaluated in these points.

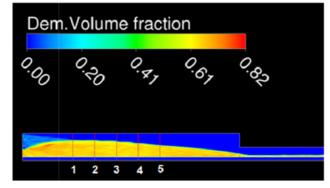


Figure 8 – Analysis positions to evaluate the bed height

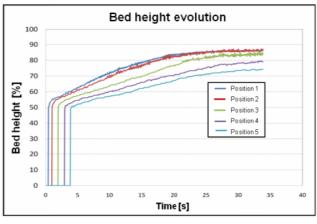


Figure 9 – Bed height time-evolution – Case 1

The simulated bed height has been compared with experimental data provided by Petrobras. The tests have been carried in a duct with equal well diameter, guaranteeing the similarity with practical gravel packing displacement operation.

The experimental tests have been carried at HALLIBURTON (MACAÉ-RJ). In order to visualize the solid flow, there were three acrylic windows, where it was possible watch the alpha and beta wave displacement and measurement. Figure 10 illustrates the equipment used in the experimental tests.



Figure 10 - Gravel packing experimental plant. (a) Acrylic window; (b) General view

The comparison between simulated and experimental data is presented in Table 1. The error between simulated and experimental data is also showed in the table and it can be observed a great agreement between simulation and experimental bed height results. These results show that CFD-DEM approach is able to supply operational data for gravel packing process design.

	Experimental Data	Simulation Data	Error
Case 1	85 %	84,74 %	-0,30 %
Case 2	84 %	82,5 %	-1,78 %
Case 3	80 %	79,61 %	-0,49 %
Case 4	79 %	81,82 %	+3,57 %

Table 1 – Simulated bed height

The CFD-DEM methodology can also determinate the fluid velocity profile and the flow regimes found in the granular system. Figure 11 illustrates a common velocity profile in the rat hole of the gravel packing process.

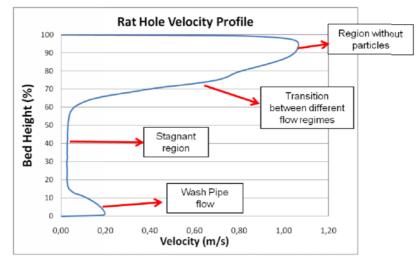


Figure 11 – Velocity profile into the rat hole

The higher velocity region is the zone where there are no particles, and the fluid flow with the critical velocity. At stagnated solid bed, the fluid suffers a big resistance to flow into the porous bed, therefore velocities in that regions are very small. Between the stagnated bed and high velocities regions, there is a flow transition regime, where there are some particles moving due the fluid drag, but the velocity is not as high as the critical velocity. At bottom, is possible observe the velocity profile flowing in the wash pipe.

3 CONCLUSIONS

CFD-DEM methodology has shown consistent results with comparison on what has been expected. The gravel packing process characteristics has been reproduced successfully through the numerical simulations.

The combination between critical velocity and bed stability supplied an alpha wave bed height that showed a great agreement with the experimental tests. The CFD-DEM approach is

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able to reproduce the phenomena that govern the horizontal solid fluid flow.

CFD-DEM approach is a promising way to test different operating conditions, evaluating bed height and also conditions where the premature screen out occurs. The mainly goal of the study is forecast the operational limits to the gravel packing process, avoiding problems during practical operations.

The next steps of the project is simulating a more realistic case, approximating the virtual experiment to the real case. In this way, some challenges must be overcome:

- Increase the number of particles inside the domain;
- Work with the real geometry (3D case);
 - Drastic increase in computational effort parallel computing.

With the fine tune of the CFD-DEM simulation methodology, these CAE softwares (Fluent + EDEM) will become a practical design tool for such cases.

REFERENCES

DEM SOLUTIONS. EDEM User Guide. 2009

DEM SOLUTIONS. EDEM Fluent Coupling Mode Guide. 2009

DEM SOLUTIONS. EDEM Training Guide. 2008.

ANSYS INC. Fluent User Guide. 2009.

- MAGALHÃES, J.V.M, Estudos para deslocamento de gravel Pack em poços horizontais extensos em cenários de óleos pesados. *ENAHPE 2006*. Domingos Martins/ES, Brazil 2006.
- MARTINS, A.L. et al. A Mechanistic Model for Horizontal Gravel Pack Displacement. SPE *European Formation Damage Conference*. Netherlands. 2003.
- ZHU, H.P. et al. Discrete Particle Simulation of Particulate Systems: Theoretical developments. *Chemical Engineering Science* 62. pag. 3378-3396. 2007.